**Amendments to the Specification:**

Please replace the paragraphs at page 9, lines 20-32 with the following rewritten paragraphs:

Reference will now be made to Figures 2 and 5, which shows a third embodiment of the present invention. This embodiment of the invention again can have an enclosure, as indicated at 60, and again includes a fuel cell stack, here indicated at 62. The stack 62 here is a closed stack, and is provided with an air pump or blower 64 connected by a main supply line 66 to an inlet of the fuel cell stack 62, and excess air exhausts from the fuel cell stack 62 as indicated at 68.

On the hydrogen side, a hydrogen supply line 70 can include a pressure gauge and a flow meter (not shown), and comprises a main hydrogen supply line 72 to the fuel cell stack 62 and a secondary supply line 74 to the catalytic burner or reactor. A solenoid valve 73 is provided in the main supply line 72, and a solenoid valve 75, a flash arrestor 76 and a non-return valve 77 are provided in the secondary line 74. A fuel purge ~~valve~~ line 78 with a controlling solenoid valve 79 are provided as for the first embodiment.

Please replace the paragraphs at page 10, lines 23-32 with the following rewritten paragraphs:

Correspondingly, to generate a heated hydrogen flow, the valve 88 is opened and the valve 89 closed. Then, excess hydrogen is supplied through the line 74, as compared to air supplied through the air supply line 80.~~main fuel line 82~~. The flow is dead ended and is only exhausted during purging when the exhaust solenoid is open. However, the flow can be controlled using control valves when not operated in dead-ended mode. In the tubular reactor 50, the oxygen in the air reacts with some of the remaining hydrogen to generate heat and moisture. The flow of hydrogen, with residual

nitrogen, together with heat and moisture, then exits from the outlet 56. This flow of heated and humidified nitrogen and hydrogen gas passes through valve 88 into the main fuel line 72.